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## Heat Transportation of Ferrofluid in a Micro Annulus

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### Abstract

*This article investigated the effect of magnetic field on heat-absorbent ferrofluid in a vertical loop consisting of a pair of concentric cylinders with surface sliding and temperature jumping. For this puprose, the control equation was converted into the dimensional form using non-dimensional quantities and parameters. The system of equations was solved analytically using an integration technique. Subsequently, the solution was obtained in the form of first and second type of Bessel functions. The results are presented graphically and show that velocity increases with the increase in the nanoparticle size. Resultantly, the rate of heat transfer of the fluid in the inner cylinder reduces.*

**Keywords:** generating/absorbing ferrofluid, inner and outer cylinder, magnetic field, vertical annulus

### Introduction

A nanofluid (NF) is a liquid carrying nanometer-sized particles called nanoparticles. The nanoparticles (NPs) utilized in NF are made up of metals, oxides, and carbides. Choi [1] was the first to introduce a new type of fluid called NF. Gorla et al. [2] have investigated NF regular convection borderline layer flow via a permeable channel on a perpendicular cone. Kuznetsov and Nield [3] have performed an analysis on natural NF flow passed through a perpendicular plate. The effect of radiation on the natural convection flow of NF has been discussed over a static perpendicular plate

by Das and Jana [4]. Pak and Cho [5] demonstrated convective heat exchange in flow regime taking  $Al_2O_3$  and  $TiO_2$  with  $H_2O$ . Nanjundappa et al [6] analyzed the effect of MHD viscosity in a ferrofluid (FF) permeable layer. A few studies have been directed at imposing convection fluid flow in microchannels. Due to its significance, such as designing and optimizing micro-machines when shipping micro-electromechanical devices, convective flow in a vertical micro-annulus has drawn a good deal of interest in industrial and technological applications. The study of the flow field at an extreme level helped to develop a method of combining fluid for micro-scale use. Jha et al [7] researched the completely advanced fluid flow in a micro-channel. Jha et al. [8] analyzed the fully advanced combined convection flow of heat-producing fluid in a vertical micro-concentric annulus cylinder. Jha and Aina [9] created a model for analyzing the impact of absorption or infusion on fully established stable laminar convection flow in a micro-annulus. Dawood et al. [10] expressed the aspects of convection flow in an upright annulus. More experimental and numerical testing can be found in the mixed convection flow by Mohammed et al. [11]. In a microchannel, Day and Stone [12] examined a rotating cylinder and reported that the cylinder and channel walls have small pores between them. The flow of stokes around a microchannel is determined by Yoon and Jeong [13]. Chen and Weng [14] numerically studied the impact of microflow on heat exchange rate. Magnetohydrodynamics (MHD) is the mutual contact of magnetic field and fluid flow. The marvels of MHD offer a few critical applications in innovative and producing fields, including MHD generators, quickening agents and pumps, stream meters and heading. Lorentz force is for the most part used to control the stream in such conditions. Sheikholeslami et al. [15] examined the magnetic impacts of finite-element methods on NF flow and thermal transport in a semi-circular yard. Sheikholeslami and Gorji-Bandpy [16] examined the mathematical solution of FF flowing. The MHD natural convection flow of NF flowing through the region between a cold external square cylinder and an inner circular heated internal is examined by Sheikholeslami et al. [17].

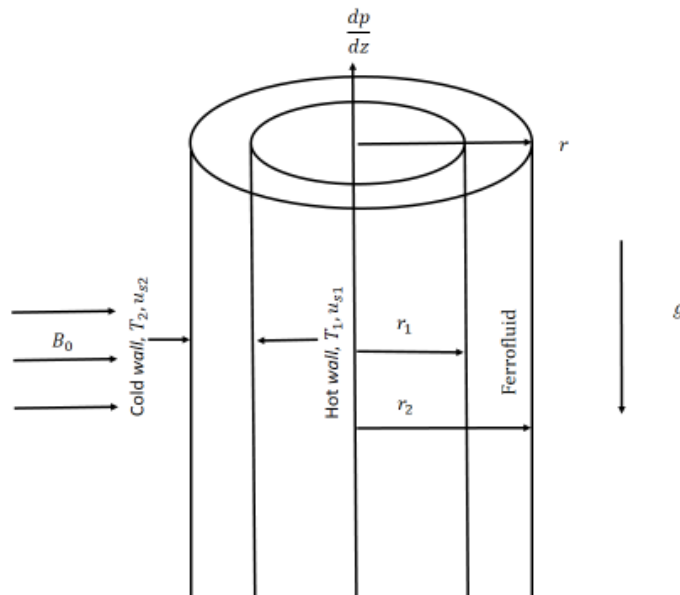
Several researchers studied the fluid flow in a vertical cylinder. Yucel [18] regarded the combination of heat and mass exchange in permeable media around a vertical cylinder. Jamil and Fetecau [19] described Maxwell

fluid flows at the border between coaxial cylinders with specified shear stress. With the presence of a static radial magnetic field, Sheikholeslami et al. [20] researched the natural convection in a concentrated annulus. Aldoss and Ali [21] looked at the combined convection from a horizontal cylinder with suction/infusion as well as a magnetic field. Lin and Shih [22] regarded the laminar boundary layer and heat exchange with constant velocity along horizontally and vertically moving cylinders and discovered that similar solutions could not be achieved owing to the curvature impact of the cylinder. The demand for heat dissipation from electronic components has been increasing for the last forty years. Tuckerman and Pease [23] are the pioneers of microchannel heat convection. They demonstrated that for small volumes microchannels have high heat flux. The impact of viscous dissipation in microtubes and microchannels was studied by Kleinstruer and Koo [24]. Sabry [25] demonstrated the impact of thermal efficiency on microchannel designs. In a microchannel, Day and Stone [26] examined a rotating cylinder, the cylinder and channel walls have small pores between them. Yoon and Jeong [27] determined the flow of stokes around a microchannel. Chen and Weng [28] studied numerically the impact of microflow on heat exchange rate. Jha et al. [29] demonstrated the impact of MHD flow in vertical micro-channel. The natural convection flow in a vertical micro-channel was demonstrated by Jha et al. [30]. Munawar et al. [31] deal with vacillate stretching cylinders. Malvandi [32] regarded NPs in the rotating sphere to report the time-dependent factor. The slip condition was used by Abbas et al. [33] to analyze unstable stretching / shrinking cylinders. Ahmad B [35,36] solve the partial differential equation (PDE) with help of the spline technique.

## 2. Problem Formulation

We assume a steady, laminar, fully developed mixed convection incompressible viscous flow in a vertical concentric annulus. We considered the infinite length of the micro-annulus. The  $r$ -axis is in the radial direction and  $z$ -axis is along upward direction. The radius of the inner and outer cylinder are  $r_1$  and  $r_2$ . The temperature of the inner and outer cylinder is  $T_1$  and  $T_2$ .  $B_0$  is the magnetic field.  $Fe_3O_4$  nanoparticles

are considered  $EG$  as a base fluid with uniform shape and size. We considered that the  $Fe_3O_4$  is Newtonian and incompressible.



**Figure1.** Geometry of the Annulus

The fluid is supposed to be single phase continuum. By assuming the Boussineq model the governing equation for laminar, two dimensional flow are

$$\frac{\mu_{nf}}{r} \frac{d}{dr} \left( r \frac{du}{dr} \right) + \beta_{nf} g \rho_{nf} (T - T_0) = \frac{dp}{dz} + \sigma_{nf} B_0^2 u, \quad (1)$$

$$\frac{1}{r} \frac{d}{dr} \left( r \frac{dT}{dr} \right) \pm \frac{Q_0 (T - T_0)}{k_{nf}} = 0. \quad (2)$$

The reference temperature is characterized in any cross sectional area of the duct as

$$T_0 = \frac{2}{r_2^2 - r_1^2} \int_{r_1}^{r_2} T(r) r dr. \quad (3)$$

The B.Cs are as following:

$$u = u_{s1} \quad \text{at } r = r_1,$$

$$\begin{aligned}
u &= u_{s_2} \text{ at } r = r_2, \\
T &= T_{s_1} \text{ at } r = r_1, \\
T &= T_{s_2} \text{ at } r = r_2.
\end{aligned} \tag{4}$$

The velocity slip is defined as

$$u_{s_1, s_2} = \pm \frac{2 - F_v}{F_v} \lambda u_r \Big|_{r=r_1, r_2} \tag{5}$$

where the temperature jump is defined as

$$T_{s_1, s_2} - T_w = \pm \frac{2 - F_t}{F_t} \frac{2\gamma}{\gamma + 1} \frac{\lambda}{(\text{Pr})_{nf}} T_r \Big|_{r=r_1, r_2} \tag{6}$$

Presenting the accompanying dimensionless parameters characterized as

$$\begin{aligned}
R &= \frac{r}{r_2}, \quad r^* = \frac{r_1}{r_2}, \quad Z = \frac{z}{\text{Re} D_h}, \quad D_h = 2(r_2 - r_1), \\
\theta &= \frac{T - T_0}{T_1 - T_2}, \quad U = \frac{u}{u_0}, \quad \text{Pr} = \frac{\mu C_p}{k}, \quad \beta_v = \frac{2 - F_v}{F_v}, \\
Kn &= \frac{\lambda}{D_h}, \quad Gr = \frac{g \beta \Delta T D_h^3}{\mu^2}, \quad \beta_t = \frac{2 - F_t}{F_t} \frac{2\gamma}{\gamma + 1} \frac{1}{\text{Pr}}, \\
w &= \frac{T_1 - T_0}{T_1 - T_2}, \quad \text{Re} = \frac{u_0 D_h}{\mu}, \quad H^2 = \frac{Q_0 r_2^2}{k}, \quad P = \frac{p}{\rho_0 u_0^2}.
\end{aligned} \tag{7}$$

The expressions for  $\mu_{nf}$ ,  $\rho_{nf}$ ,  $\alpha_{nf}$ ,  $\beta_{nf}$ ,  $\sigma_{nf}$ ,  $(\rho c_p)_{nf}$  and  $k_{nf}$  are expressed

$$\begin{aligned}
\alpha_{nf} &= \frac{k_{nf}}{(\rho C_p)_{nf}}, \quad \rho_{nf} = (1 - \phi) \rho_f + \phi \rho_s, \quad \mu_{nf} = \frac{\mu_f}{(1 - \phi)^{2.5}}, \\
\text{as } \frac{k_{nf}}{k_f} &= \frac{k_s + 2k_f - 2\phi(k_f - k_s)}{k_s + 2k_f + \phi(k_f - k_s)}, \quad (\rho C_p)_{nf} = (1 - \phi)(\rho C_p)_s, \\
\beta_{nf} &= (1 - \phi) \beta_f + \phi \beta_s, \quad \frac{\sigma_{nf}}{\sigma_f} = 1 + \frac{3\phi \left( \frac{\sigma_s}{\sigma_f} - 1 \right)}{\left( \frac{\sigma_s}{\sigma_f} + 2 \right) - \phi \left( \frac{\sigma_s}{\sigma_f} - 1 \right)}.
\end{aligned} \tag{8}$$

**Table 1.** Thermo-physical Properties of *NFs* and *NPs* .

| <b>Liquids and nano particles</b> | $\rho(Kg/m^3)$ | $c_p(k/kg)$ | $k(wK/m)$ | $\beta*10^{-5}(K^{-1})$ | $\sigma(S/m)$  |
|-----------------------------------|----------------|-------------|-----------|-------------------------|----------------|
| EG                                | 113.2          | 2410        | 0.252     | 1.89                    | $1.07*10^{-6}$ |
| $Fe_3O_4$                         | 5200           | 670         | 6         | 0.5                     | 25000          |

Using quantities given in (7)&(8) Eqs. (1) and (2) in dimensionless form are

$$\frac{1}{R} \frac{d}{dR} \left( R \frac{dU}{dR} \right) + \frac{\phi_1}{A} \frac{Gr}{Re} \theta - \frac{1}{A} \frac{dP}{dZ} - \phi_4 A_3 M^2 U = 0, \quad (9)$$

$$\frac{1}{R} \frac{d}{dR} \left( R \frac{d\theta}{dR} \right) \pm \frac{1}{A_1} H^2 \theta = 0, \quad (10)$$

The BCs are

$$U = 2\beta_v Kn(1-r^*) \frac{dU}{dR} \quad \text{at} \quad R = r^*, \quad (11)$$

$$U = -2\beta_v Kn(1-r^*) \frac{dU}{dR} \quad \text{at} \quad R = 1, \quad (12)$$

$$\theta = \frac{T_{s_1} - T_0}{T_1 - T_2} = w + 2A_2 \beta_T Kn(1-r^*) \frac{d\theta}{dR} \quad \text{at} \quad R = r^*, \quad (13)$$

$$\theta = \frac{T_{s_2} - T_0}{T_2 - T_0} = w - 1 - 2A_2 \beta_T Kn(1-r^*) \frac{d\theta}{dR} \quad \text{at} \quad R = 1, \quad (14)$$

Where 
$$A_2 = \frac{\phi_1 A_1}{\phi_3}.$$

From Eqs. (5) and (10), we obtained the following temperature constraints

$$\int_{r^*}^1 \theta(R) R dR = 0 \quad (15)$$

## 2.1. Analytical Solution

It can be noted that the solution for  $\theta$  is different for  $+H$  in Eq.(10) from  $-H$  in Eq.(10). Two cases of solutions are formed.

### 2.1.1. Case I: Heat Generating Fluid (source)

The closed form solution for Eq. (10) with BCs given in Eqs. (13), (14) and (15) is

$$\theta(R) = \frac{A_5 Y_0(E_1 R) - A_6 J_0(E_1 R)}{(x_2 - x_4) A_5 - (x_1 - x_3) A_6}. \quad (16)$$

By using Eq. (16) into Eq. (9) and integrating any applying B.Cs shown in Eq. (11) and Eq. (12)

$$U(R) = E_3 \left( \phi_1 \frac{Gr}{Re} \left( \frac{A_5 Y_0(E_1 R) - A_6 J_0(E_1 R)}{(x_2 - x_4) A_5 - (x_1 - x_3) A_6} \right) - \frac{dP}{dZ} \right) + C_1 I_0(E_2 R) + C_2 K_0(E_2 R). \quad (17)$$

The mean velocity  $u_0$  for any cross sectional area in the channel is

$$u_0 = \frac{\int_{r^*}^1 U(R) R dR}{\int_{r^*}^1 R dR} = 1. \quad (18)$$

The dimensionless  $\theta_b$  can be defined as

$$\theta_b = \frac{T_b - T_0}{T_1 - T_2} = \frac{2}{(1 - r^{*2})} \int_{r^*}^1 R U(R) \theta(R) dR \quad (19)$$

By using Eq. (16) the convective heat exchange for inner/ outer cylinder is

$$h = \frac{-k \frac{dT}{dr} \Big|_{r=r_1}}{T_1 - T_b}. \quad (20)$$

$$h = \frac{-k \frac{dT}{dr} \Big|_{r=r_2}}{T_2 - T_b}. \quad (21)$$

$Nu_1$  at the outer/inner surfaces of inner/outer cylinder is

$$Nu_1 = \frac{2(1 - r^*) \frac{d\theta}{dR} \Big|_{R=r^*}}{\theta_b - w}. \quad (22)$$

$$Nu_2 = \frac{2(1 - r^*) \frac{d\theta}{dR} \Big|_{R=1}}{\theta_b + 1 - w}. \quad (23)$$

The velocity of the outer and inner surface

$$\frac{dU}{dR} \Big|_{R=r^*} = 0 \quad \text{and} \quad \frac{dU}{dR} \Big|_{R=1} = 0. \quad (24)$$



The  $Gr/Re$  for  $+H$  from Eq. (24) for the outer/inner surface of the outer/inner cylinder is given as

$$\left. \frac{Gr}{Re} \right|_{R=r^*} = \frac{x_{34}}{x_{33}} \quad \text{and} \quad \left. \frac{Gr}{Re} \right|_{R=1} = \frac{x_{37}}{x_{36}}. \quad (25)$$

### 2.1.2. Case II: Heat Absorbing Fluid (sink)

The closed form solution for Eq. (10) with BCs given in Eqs. (13), (14) and (15) is

$$\theta(R) = \frac{A_7 I_0(E_1 R) - A_8 K_0(E_1 R)}{(x_{40} - x_{41}) A_8 - (x_{38} - x_{39}) A_7}. \quad (26)$$

The  $U(R)$  can be written as

$$U(R) = E_3 \left( \phi \frac{Gr}{Re} \left( \frac{A_7 I_0(E_1 R) - A_8 K_0(E_1 R)}{(x_{40} - x_{41}) A_8 - (x_{38} - x_{39}) A_7} \right) - \frac{dP}{dZ} \right) + C_3 I_0(E_2 R) + C_4 K_0(E_2 R). \quad (27)$$

At last  $Gr/Re$  for the case of sink from Eq. (24) is as under

$$\left. \frac{Gr}{Re} \right|_{R=r^*} = \frac{x_{63}}{x_{62}} \quad \text{and} \quad \left. \frac{Gr}{Re} \right|_{R=1} = \frac{x_{70}}{x_{69}}. \quad (28)$$

## 3. Results and Discussion

The results for  $U(R)$ ,  $\theta(R)$ ,  $Nu$  are discussed and the graphs are shown in Figures 2 - 11 so that the effect of each parameter can be seen.

From Figure 2 we examined the impact of  $\phi$  on  $\theta(R)$  for the case of  $+H$  and  $-H$ . In Figure 2 for case  $+H$  and  $-H$  the  $\theta(R)$  enhances with enhance in  $\phi$ . Figure 3 shows the influence of  $+H$  and  $-H$  on  $\theta$ . From the Figure, we can see that  $\theta(R)$  increases by increasing  $+H$  and decreases in the case of  $-H$ . Figure 4 shows the effect of  $\phi$  on  $U(R)$ . We see from the fig. that  $U(R)$  increases for  $\phi$  in both cases  $+H$  and  $-H$ . Figure 5 is graphed to show the influence of  $Kn$  on  $U(R)$ . From the Figures, we see that velocity enhances with increase in  $Kn$  for both cases  $+H$  and  $-H$ . It

is noted that the  $u_{s_1, s_2}$  on surface of the cylinders increases for both  $+H$  and  $-H$  case, as the amount of  $Kn$  rises, the retarding impact of the cylinder reduces. Figure 6 shows the effect of  $M$  on  $U(R)$ . It can be noted that the velocity enhances with increase in  $M$  for both cases of  $+H$  and  $-H$ . The variation in  $Gr/Re$  is shown in Figure 7. we can see that the  $U(R)$  increases with increase in  $Gr/Re$  for both cases  $+H$  and  $-H$ . It is noted that for  $\pm H$ , enhancing  $Gr/Re$  leads to an increase in  $U(R)$  on the outer surface of the inner cylinder where the result is simply increased on the outer cylinder's inner surface.

Figure 8 shows the effect of  $H$  on  $Nu_1$ . we can see that the  $Nu_1$  increases with increase in  $H$  for both cases of (a) and (b). Figure 9 shows the impact of  $H$  on  $Nu_2$ . We can see that the  $Nu_2$  increases with increase in  $H$  for both cases of (a) and (b). The variation in  $\phi$  is shown in Figure. 10 for the case of  $Nu_1$ . The figure shows that the  $Nu_1$  decreases for both cases in  $\phi$ . The variation in  $\phi$  is shown in Figure 11 for the case of  $Nu_2$ . The Figure shows that  $Nu_2$  increases with increase in  $\phi$  for both cases.

#### 4. Conclusions

This paper presented the analysis of heat exchange for ferrofluid in a micro annulus. The impact of the  $M$ ,  $\phi$ ,  $H$ ,  $Gr/Re$ ,  $Kn$ ,  $r^*$  on the  $U(R)$ ,  $\theta(R)$  and  $Nu$  are expressed as:

- $\theta(R)$  increases when  $\phi$  increases for heat generating/absorbing fluid.
- $\theta(R)$  increases when  $H$  increases.
- $U(R)$  increases when  $\phi$  increases for heat generating/absorbing fluid.
- $U(R)$  increases when  $Kn$  increases for heat generating/absorbing fluid.
- $U(R)$  increases when  $M$  increases for heat generating/absorbing fluid.
- $U(R)$  increases when  $Gr/Re$  increases for heat generating/absorbing fluid.
- $Nu$  for inner cylinder decreases when  $\phi$  increases for heat generating/absorbing fluid.

- $Nu$  increases when  $\phi$  increases for both cases heat generating/absorbing fluid.

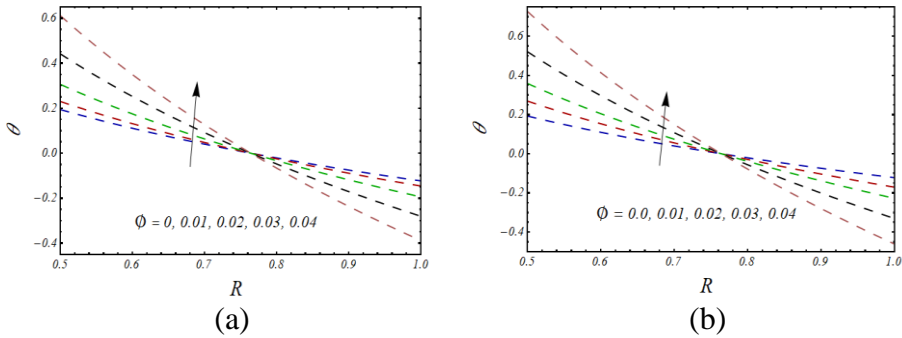


Figure 2. (a)  $\theta$  (b)  $\theta$  for  $\phi$ .

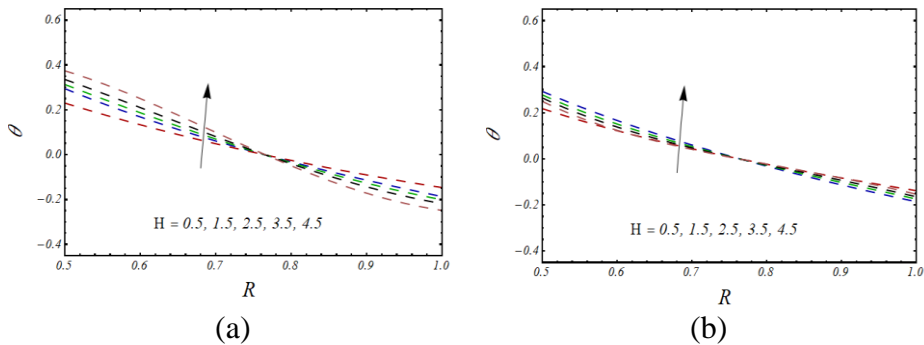


Figure 3. (a)  $\theta$  (b)  $\theta$  for  $H$ .

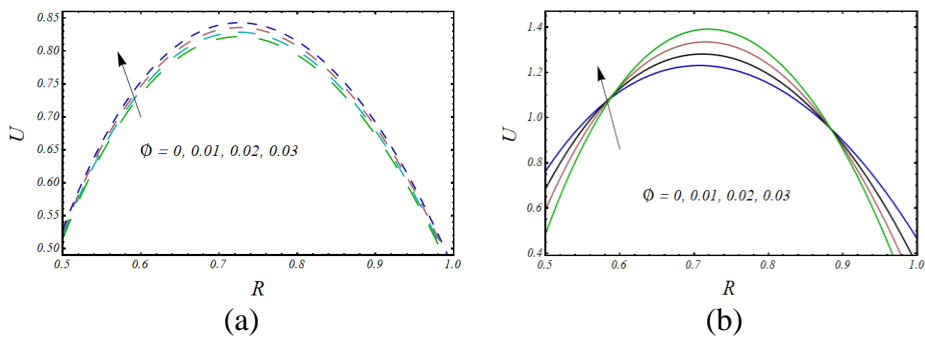
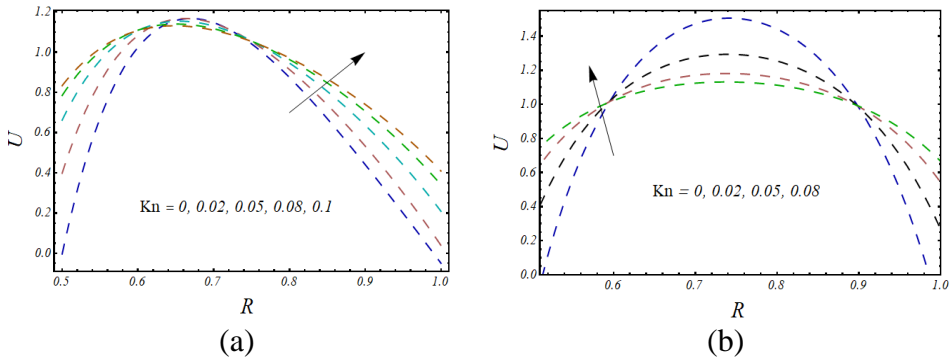
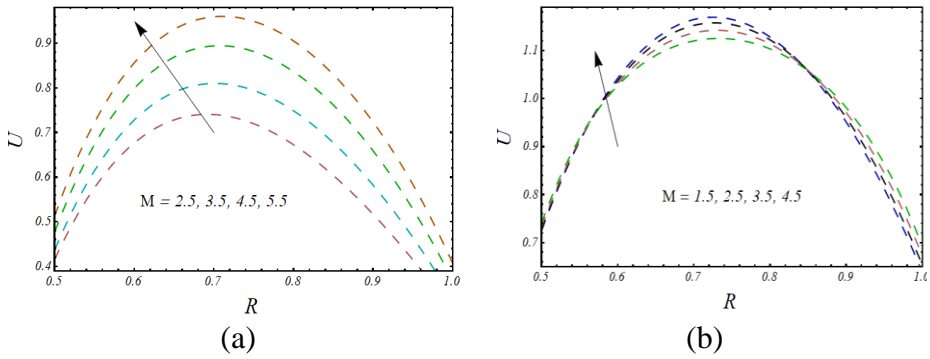


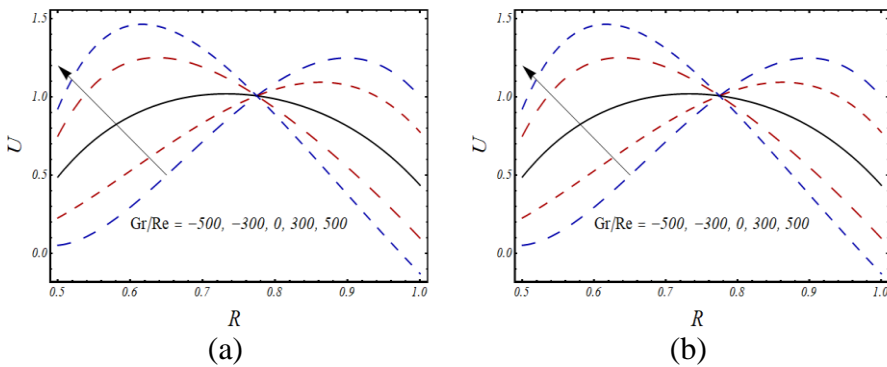
Figure 4. (a)  $U$  (b)  $U$  for  $\phi$ .



**Figure 5.** (a)  $U$  (b)  $U$  for  $Kn$ .



**Figure 6.** (a)  $U$  (b)  $U$  for  $M$ .



**Figure 7.** (a)  $U$  (b)  $U$  for  $Gr/Re$ .

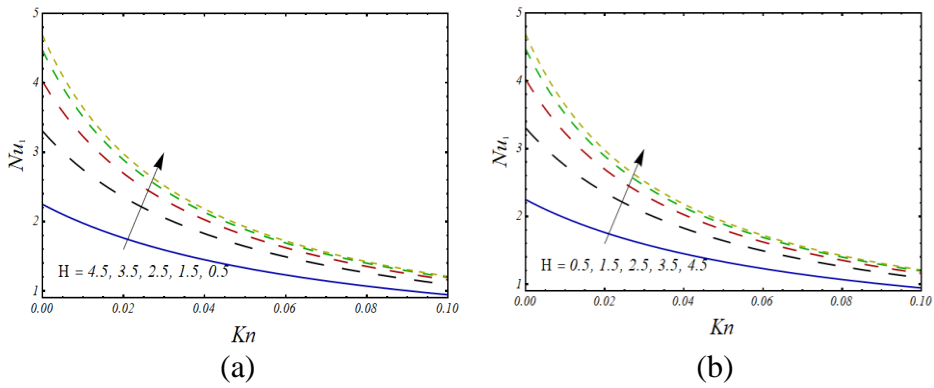


Figure 8. (a)  $Nu_1$  (b)  $Nu_1$  for  $H$ .

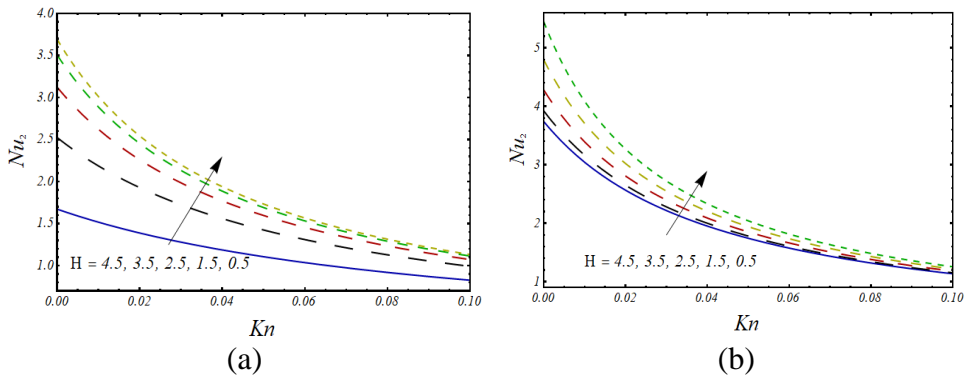


Figure 9. (a)  $Nu_2$  (b)  $Nu_2$  for  $H$ .

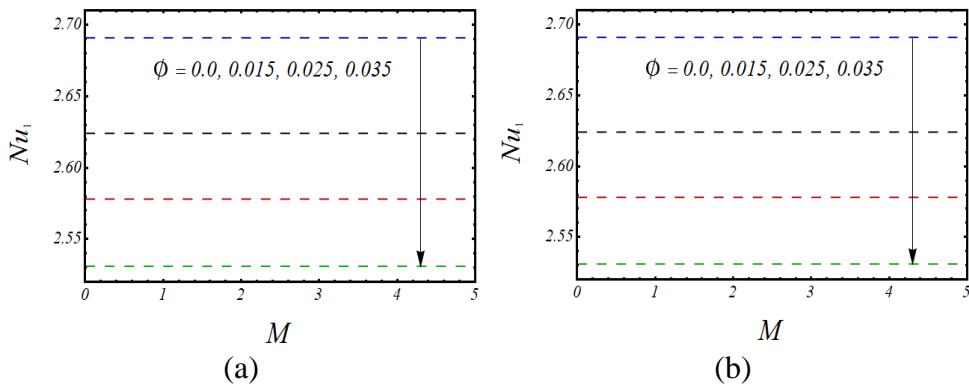
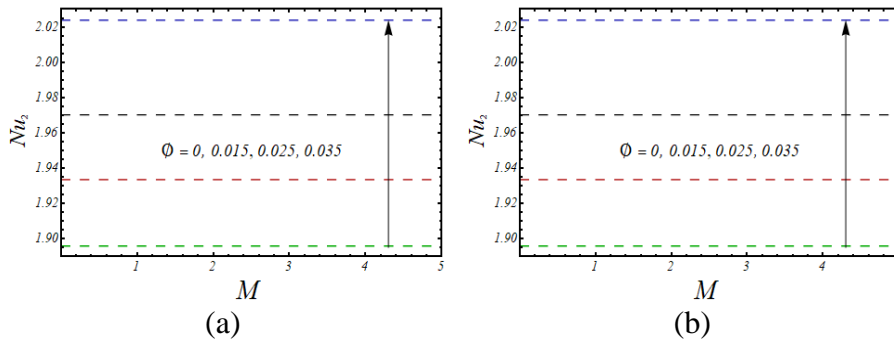


Figure 10. (a)  $Nu_1$  (b)  $Nu_1$  for  $\phi$ .



**Figure 11.** (a)  $Nu_2$  (b)  $Nu_2$  for  $\phi$ .

**Competing Interests:** The authors declare no conflict of interest.

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### Appendix

$$A = 4(1-r^*)^2, \quad \phi_1 = (1-\phi)^{2.5} \left( 1 - \phi + \frac{\phi\rho_s}{\rho_f} \right), \quad \phi_2 = 1 - \phi + \frac{\phi\rho_s}{\rho_f},$$

$$\phi_3 = 1 - \phi + \frac{(\rho c_p)_s}{(\rho c_p)_f}, \quad \phi_4 = (1-\phi)^{2.5}, \quad A_1 = \frac{k_{nf}}{k_f} = \frac{k_s + 2k_f - 2\phi(k_f - k_s)}{k_s + 2k_f + 2\phi(k_f - k_s)}$$

$$A_3 = \frac{\sigma_{nf}}{\sigma_f} = 1 + \frac{3\phi \left( \frac{\sigma_s}{\sigma_f} - 1 \right)}{\left( \frac{\sigma_s}{\sigma_f} + 2 \right) - \phi \left( \frac{\sigma_s}{\sigma_f} - 1 \right)}, \quad A = 4(1-r^*)^2,$$

$$\phi_1 = (1-\phi)^{2.5} \left( 1 - \phi + \frac{\phi\rho_s}{\rho_f} \right), \quad \phi_2 = 1 - \phi + \frac{\phi\rho_s}{\rho_f}, \quad \phi_3 = 1 - \phi + \frac{(\rho c_p)_s}{(\rho c_p)_f},$$

$$\phi_4 = (1-\phi)^{2.5}, \quad A_1 = \frac{k_{nf}}{k_f} = \frac{k_s + 2k_f - 2\phi(k_f - k_s)}{k_s + 2k_f + 2\phi(k_f - k_s)}$$

$$A_3 = \frac{\sigma_{nf}}{\sigma_f} = 1 + \frac{3\phi \left( \frac{\sigma_s}{\sigma_f} - 1 \right)}{\left( \frac{\sigma_s}{\sigma_f} + 2 \right) - \phi \left( \frac{\sigma_s}{\sigma_f} - 1 \right)}.$$

$$E_1^2 = \frac{H^2}{A_1}, \quad E_2^2 = \phi_4 A_3 M^2, \quad C_1 = \frac{1}{x_{19}} \left( E_3 x_{18} \frac{dP}{dZ} + E_3 E_4 x_{17} \frac{Gr}{Re} \right),$$

$$C_2 = \frac{1}{x_{22}} \left( E_3 x_{21} \frac{dP}{dZ} + E_3 E_4 x_{20} \frac{Gr}{Re} \right), \quad \frac{dP}{dZ} = \frac{Gr}{Re} \frac{x_{26}}{x_{27}} - \frac{1}{E_3 x_{27}},$$

$$A_5 = J_1(E_1) - r^* J_1(E_1 r^*), \quad A_6 = Y_1(E_1) - r^* Y_1(E_1 r^*),$$

$$x_1 = J_0(E_1 r^*) + 2A_2 \beta_t k_n (1-r^*) E_1 J_1(E_1 r^*),$$

$$x_2 = Y_0(E_1 r^*) + 2A_2 \beta_t k_n (1-r^*) E_1 Y_1(E_1 r^*),$$

$$x_3 = J_0(E_1) - 2A_2 \beta_t k_n (1-r^*) E_1 J_1(E_1),$$

$$x_4 = Y_0(E_1) - 2A_2 \beta_t k_n (1-r^*) E_1 Y_1(E_1),$$

$$\begin{aligned}
 x_5 &= J_1(E_1) - r^* J_1(E_1 r^*), \quad x_6 = Y_1(E_1) - r^* Y_1(E_1 r^*), \\
 x_7 &= I_0(E_2 r^*) - 2\beta_v k_n (1-r^*) E_2 I_1(E_2 r^*), \\
 x_8 &= K_0(E_2 r^*) + 2\beta_v k_n (1-r^*) E_2 K_1(E_2 r^*), \\
 x_9 &= Y_0(E_1 r^*) + 2\beta_v k_n (1-r^*) E_1 Y_1(E_1 r^*), \\
 x_{10} &= J_0(E_1 r^*) + 2\beta_v k_n (1-r^*) E_1 J_1(E_1 r^*), \\
 x_{11} &= I_0(E_2) + 2\beta_v k_n (1-r^*) E_2 I_1(E_2), \\
 x_{12} &= K_0(E_2) - 2\beta_v k_n (1-r^*) E_2 K_1(E_2), \\
 x_{13} &= Y_0(E_1) - 2\beta_v k_n (1-r^*) E_1 Y_1(E_1), \\
 x_{14} &= J_0(E_1) - 2\beta_v k_n (1-r^*) E_1 J_1(E_1), \quad x_{15} = x_5 x_9 - x_6 x_{10}, \quad x_{16} = x_5 x_{13} - x_6 x_{14}, \\
 x_{17} &= x_8 x_6 - x_{12} x_{15}, \quad x_{18} = x_{12} - x_8, \quad x_{19} = x_7 x_{12} - x_8 x_{11}, \quad x_{20} = x_7 x_{16} - x_{11} x_{15}, \\
 x_{21} &= x_{11} - x_7, \quad x_{22} = x_8 x_{11} - x_7 x_{12}, \quad x_{23} = I_1(E_2) - r^* I_1(E_2 r^*), \\
 x_{24} &= K_1(E_2) - r^* K_1(E_2 r^*), \quad x_{25} = \frac{2}{E_2(1-r^{*2})}, \\
 x_{26} &= \frac{E_4 x_{25} (x_{17} x_{22} x_{23} - x_{19} x_{20} x_{24})}{x_{19} x_{22}}, \quad x_{27} = \frac{x_{19} x_{22} - x_{25} (x_{18} x_{22} x_{23} - x_{19} x_{20} x_{24})}{x_{19} x_{22}}, \\
 x_{28} &= E_2 \left( \frac{E_4 x_{17}}{x_{19}} + \frac{x_{18} x_{26}}{x_{19} x_{27}} \right), \quad x_{29} = E_2 \left( \frac{E_4 x_{20}}{x_{22}} + \frac{x_{21} x_{26}}{x_{22} x_{27}} \right) \quad x_{30} = \frac{E_2 x_{18}}{E_3 x_{19} x_{27}}, \\
 x_{31} &= \frac{E_2 x_{21}}{E_3 x_{22} x_{27}}, \\
 x_{32} &= x_5 Y_1(E_1 r^*) - x_6 J_1(E_1 r^*), \quad x_{33} = x_{28} I_1(E_2 r^*) - x_{29} K_1(E_2 r^*) - E_1 E_4 x_{32}, \\
 x_{34} &= x_{30} I_1(E_2 r^*) - x_{31} K_1(E_2 r^*), \quad x_{35} = x_5 Y_1(E_1) - x_6 J_1(E_1), \\
 x_{36} &= x_{28} I_1(E_2) - x_{29} K_1(E_2) - E_1 E_4 x_{35}, \quad x_{37} = x_{30} I_1(E_2) - x_{31} K_1(E_2), \\
 E_3 &= \frac{1}{A E_2^2}, \quad E_4 = \frac{\phi_1}{x}, \quad E_5 = \frac{\phi_1}{x_{44}}, \quad C_3 = \frac{1}{x_{49}} \left( E_3 x_{51} \frac{dP}{dZ} + E_3 E_5 x_{50} \frac{Gr}{Re} \right),
 \end{aligned}$$

$$\begin{aligned}
C_4 &= \frac{1}{x_{52}} \left( E_3 x_{54} \frac{dP}{dZ} + E_3 E_5 x_{53} \frac{Gr}{Re} \right), \quad \frac{dP}{dZ} = \frac{Gr}{Re} \frac{x_{55}}{x_{56}} - \frac{1}{E_3 x_{56}}, \\
A_7 &= K_1(E_1) - r^* K_1(E_1 r^*), \quad A_8 = I_1(E_1) - r^* I_1(E_1 r^*), \\
x_{38} &= I_0(E_1 r^*) - 2A_2 \beta_t k_n (1-r^*) E_1 I_1(E_1 r^*), \\
x_{39} &= I_0(E_1) + 2A_2 \beta_t k_n (1-r^*) E_1 I_1(E_1), \\
x_{40} &= K_0(E_1 r^*) + 2A_2 \beta_t k_n (1-r^*) E_1 K_1(E_1 r^*), \\
x_{41} &= K_0(E_1) - 2A_2 \beta_t k_n (1-r^*) E_1 K_1(E_1), \quad x_{42} = I_1(E_1) - r^* I_1(E_1 r^*), \\
x_{43} &= K_1(E_1) - r^* K_1(E_1 r^*), \quad x_{45} = I_0(E_1 r^*) - 2\beta_v k_n (1-r^*) E_1 I_1(E_2 r^*), \\
x_{46} &= K_0(E_1 r^*) + 2\beta_v k_n (1-r^*) E_1 K_1(E_1 r^*), \\
x_{47} &= I_0(E_1) + 2\beta_v k_n (1-r^*) E_1 I_1(E_1), \\
x_{48} &= K_0(E_1) - 2\beta_v k_n (1-r^*) E_1 K_1(E_1), \quad x_{49} = x_7 x_{12} - x_8 x_{11}, \\
x_{50} &= x_8 (x_{43} x_{47} + x_{42} x_{48}) - x_{12} (x_{43} x_{45} - x_{42} x_{46}), \quad x_{51} = x_{12} - x_8, \\
x_{52} &= x_8 x_{11} - x_7 x_{12}, \quad x_{53} = x_7 (x_{43} x_{47} + x_{42} x_{48}) - x_{11} (x_{43} x_{45} - x_{42} x_{46}), \\
x_{54} &= x_{11} - x_7, \quad x_{55} = \frac{E_5 x_{25} (x_{23} x_{50} x_{52} - x_{24} x_{49} x_{53})}{x_{49} x_{52}}, \\
x_{56} &= 1 - \frac{x_{25} (x_{23} x_{51} x_{52} - x_{24} x_{49} x_{54})}{x_{49} x_{52}}, \quad x_{57} = E_2 \left( \frac{E_5 x_{50}}{x_{49}} + \frac{x_{51} x_{55}}{x_{49} x_{56}} \right), \\
x_{58} &= E_2 \left( \frac{E_5 x_{53}}{x_{52}} + \frac{x_{54} x_{55}}{x_{52} x_{56}} \right), \quad x_{59} = \frac{E_2 x_{51}}{E_3 x_{49} x_{56}}, \quad x_{60} = \frac{E_2 x_{54}}{E_3 x_{52} x_{56}}, \\
x_{61} &= x_{43} I_1(E_1 r^*) - x_{42} K_1(E_1 r^*), \quad x_{62} = x_{57} I_1(E_2 r^*) - x_{58} K_1(E_2 r^*) - E_1 E_5 x_{61}, \\
x_{63} &= x_{59} I_1(E_2 r^*) - x_{60} K_1(E_2 r^*), \quad x_{64} = x_{43} I_1(E_1) - x_{42} K_1(E_1), \\
x_{65} &= \frac{x_{51}}{E_3 x_{49} x_{56}}, \quad x_{66} = \frac{x_{54}}{E_3 x_{52} x_{56}}, \quad x_{67} = x_{57} I_1(E_2) - x_{58} K_1(E_2) + E_1 E_5 x_{64}, \\
x_{68} &= x_{65} I_1(E_2) - x_{66} K_1(E_2).
\end{aligned}$$

## Nomenclature

|           |  |                    |   |
|-----------|--|--------------------|---|
| $b$       | Body force   | $U$                | Dimensionless axial velocity                        |
| $C_p$     | Specific heat at constant pressure                               | $V$                | Velocity field                                      |
| $D_h$     | Hydraulic diameter   | $w$                | Ratio of wall temperature                           |
| $F_v$     | Tangential momentum accommodation coefficient                    | $z, r$             | Axial and radial coordinate, respectively           |
| $F_t$     | Thermal accommodation coefficient                                | $Z, R$             | Dimensionless axial and radial coordinate,          |
| $g$       | Gravitational acceleration                                       |                    | <b>Greeks letters</b>                               |
| $Gr$      | Grashof number   | $\tau$             | Cauchy stress tensor                                |
| $Gr / Re$ | Mixed convection parameter                                       | $\alpha$           | Thermal diffusivity of the fluid                    |
| $h$       | Convective heat transfer coefficient                             | $\beta$            | Coefficient of thermal expansion                    |
| $\pm H$   | Dimensionless heat generation or absorption parameter            | $\beta_v, \beta_t$ | Dimensionless variables                             |
| $k$       | Thermal conductivity of the fluids                               | $\gamma$           | Ratio of specific heat                              |
| $Kn$      | Knudsen number   | $\lambda$          | Molecular mean free path                            |
| $Nu_1$    | Rate of heat transfer at the outer surface of the inner cylinder | $\mu$              | Dynamic viscosities of the phases                   |
| $Nu_2$    | Rate of heat transfer at the inner surface of the outer cylinder | $\rho$             | Density   |
| $P$       | Pressure difference  | $\nu$              | Fluid kinematic viscosity fluid kinematic viscosity |
| Pr        | Prandtl number   | $\theta$           | Dimensionless temperature                           |
| $Q_0$     | Dimensional heat generation parameter                            | $\theta_b$         | Bulk temperature                                    |
| Re        | Reynolds number  | $\phi$             | Dimensionless concentration                         |
| $r^*$     | Ration of radiuses   | $\sigma$           | Electrical conductivity                             |
| $r_1$     | Radius of the inner cylinder                                     | $\mu_{nf}$         | Effective dynamic viscosity                         |
| $r_2$     | Radius of the outer cylinder                                     | $(\rho C_p)_{nf}$  | Heat capacitance                                    |
| $s_1$     | Fluid properties on the inner cylinder                           | $k_{nf}$           | Thermal conductivity                                |
| $s_2$     | Fluid properties on the outer cylinder                           | $\rho_{nf}$        | Effective density                                   |
| $T$       | Temperature of the fluid   | $\alpha_{nf}$      | Thermal diffusivity                                 |
| $T_0$     | Reference temperature of the fluid                               | $\mu_f$            | Dynamic viscosity                                   |

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|       |  |          |  |
|-------|--|----------|--|
| $T_1$ | Temperature at outer surface of the inner cylinder | $\rho_f$ | Density for ferrofluid                 |
| $T_2$ | Temperature at inner surface of the outer cylinder | $\rho_s$ | Density for base fluid                 |
| $T_w$ | Wall temperature                                   | $k_s$    | Thermal conductivity of solid particle |
| $u_0$ | Mean velocity                                      | $k_f$    | Thermal conductivity of fluid          |
| $u$   | Axial velocity                                     |          |  |